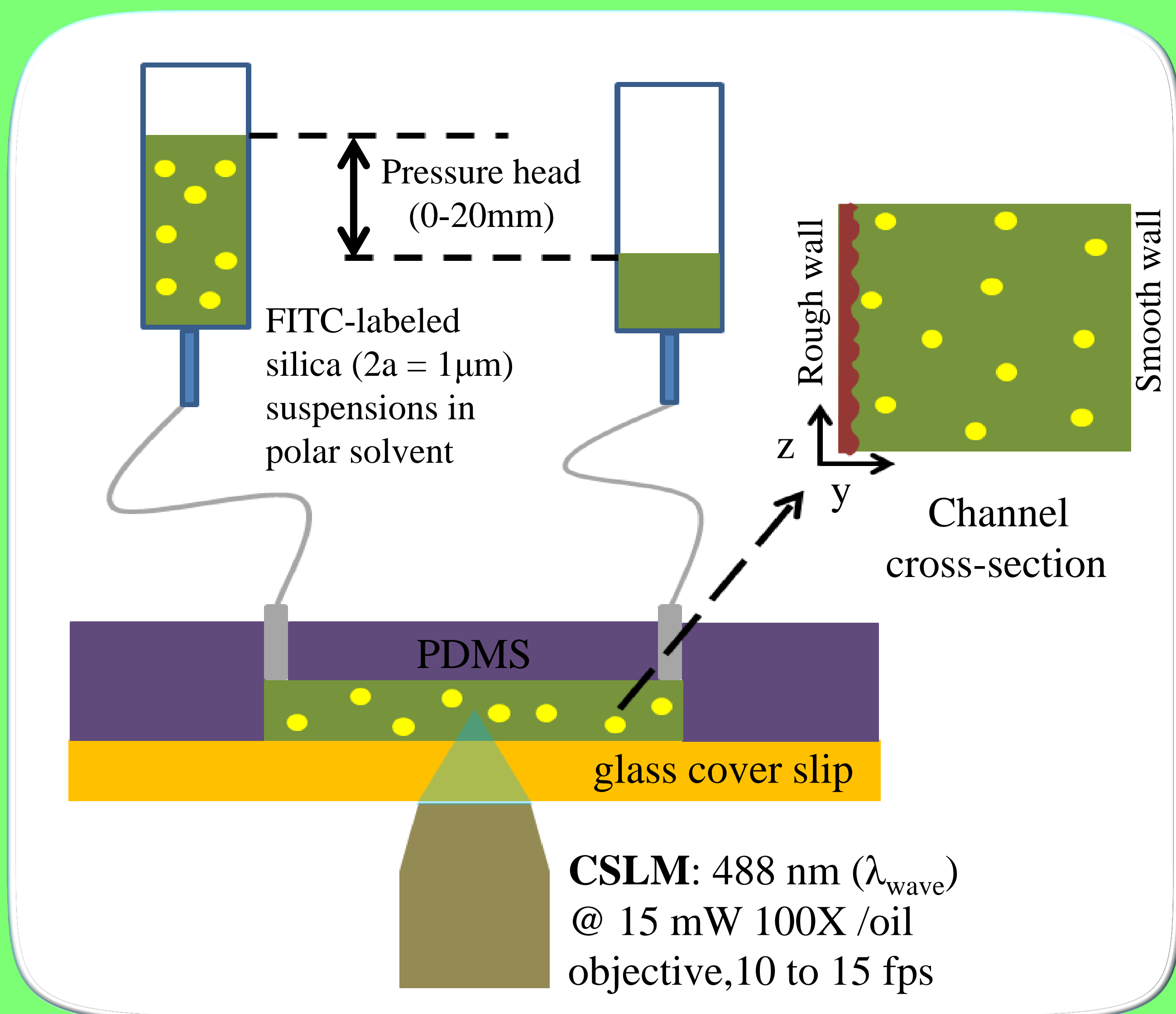
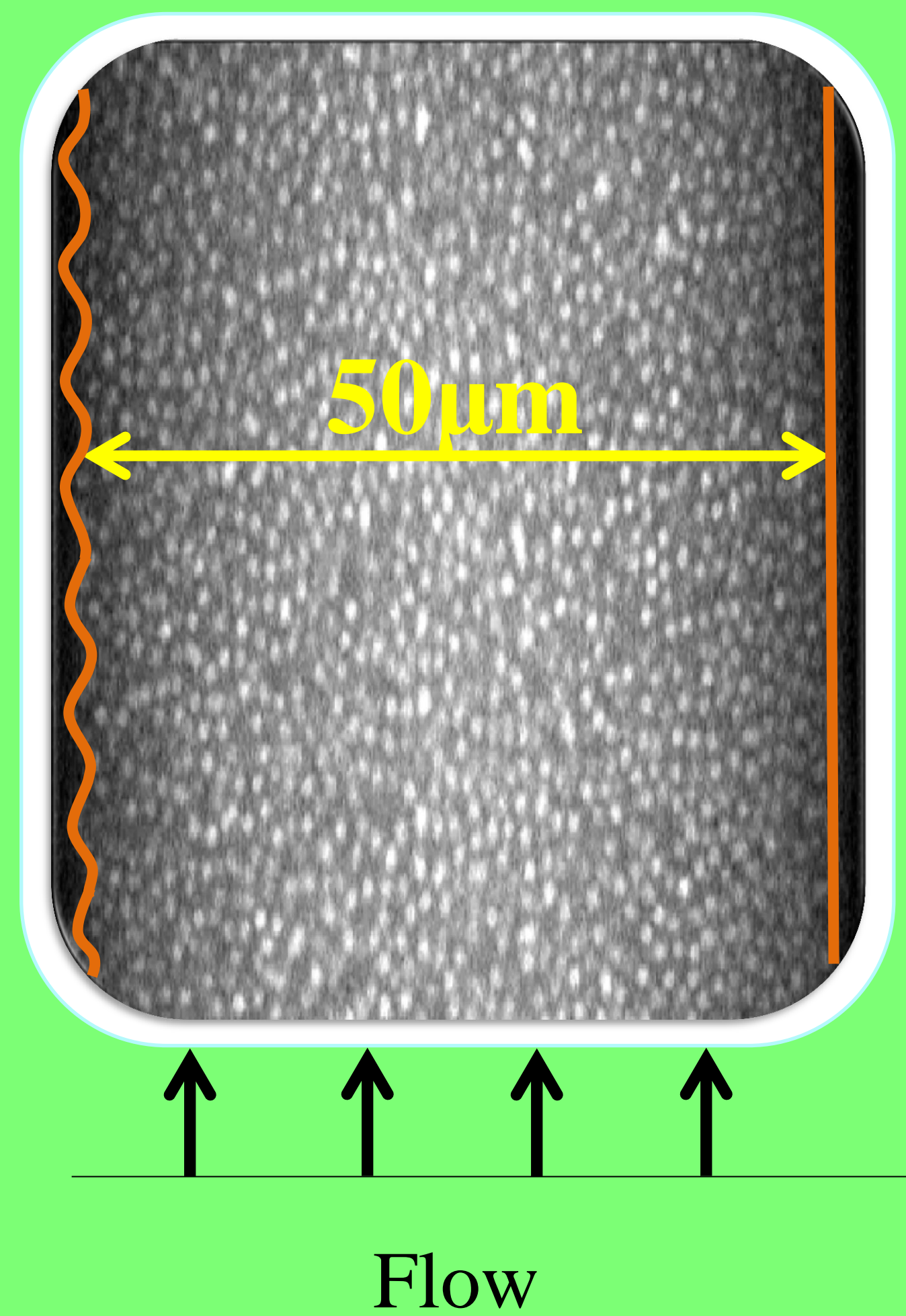


## Introduction

While colloidal hard sphere suspensions are well-known as model fluids, much less is known about their behavior when they are made to flow through microchannels. We have initiated a study into the spheres' spatial distribution, flow profile and (apparent) diffusive behavior, as a function of the volume fraction (0.01-0.4), and the Péclet number (0 to 40) which indicates the strength of the shear flow as compared to Brownian motion:  $Pe = \frac{6\pi\eta_0\gamma'a^3}{kT}$ . Cross-sectional channel dimensions are taken 30-50 particle diameters, while also the roughness of the wall is varied. After confocal microscopy measurements, the particles' positions and displacements are analyzed using (adapted) tracking codes written in IDL language.



## Experiments



### solvents:

1. Methanol + Bromoform (low viscous)
  2. Water + Glycerol (high viscous)
- both refractive index matching for silica solvent 1 is also density-matching.

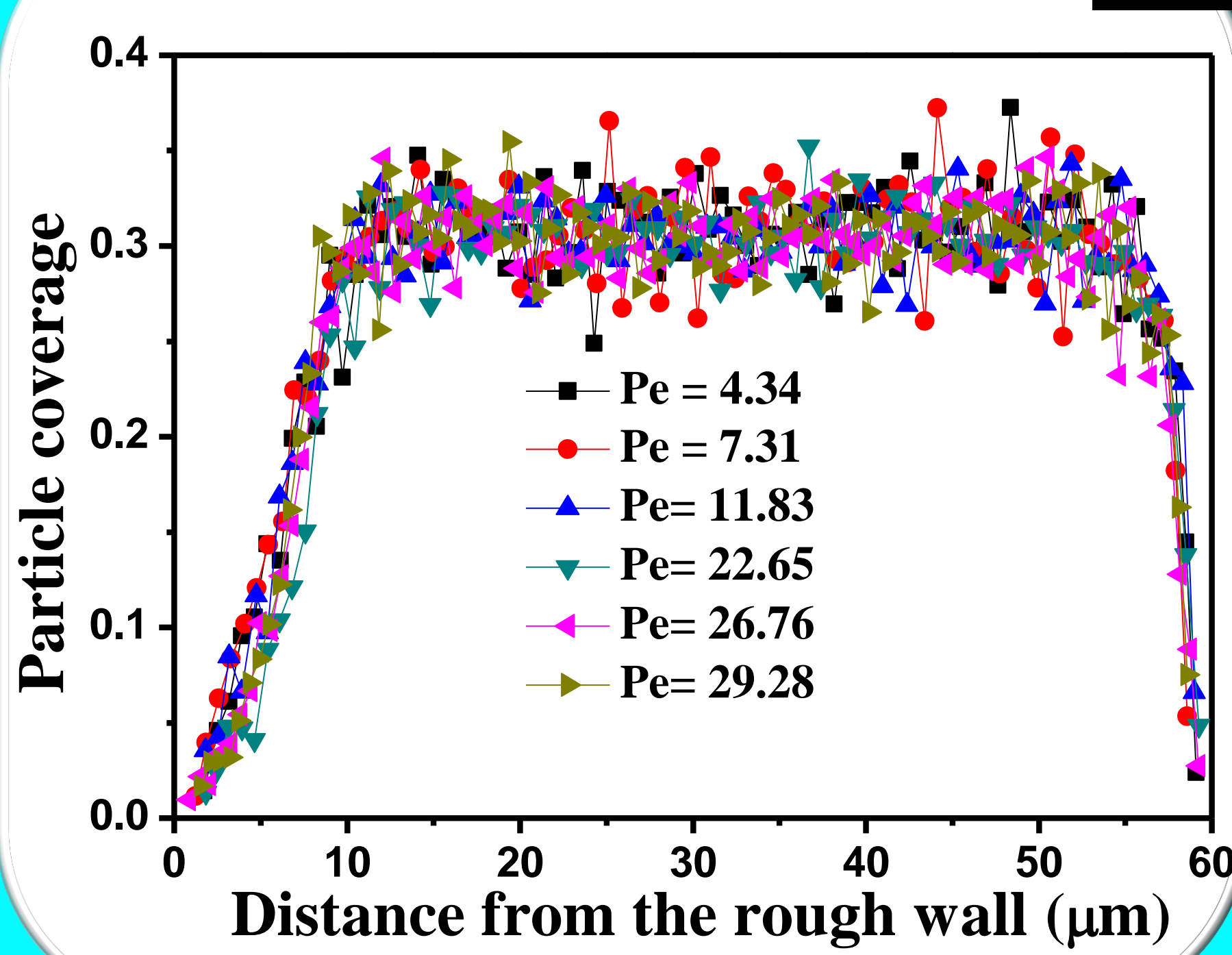
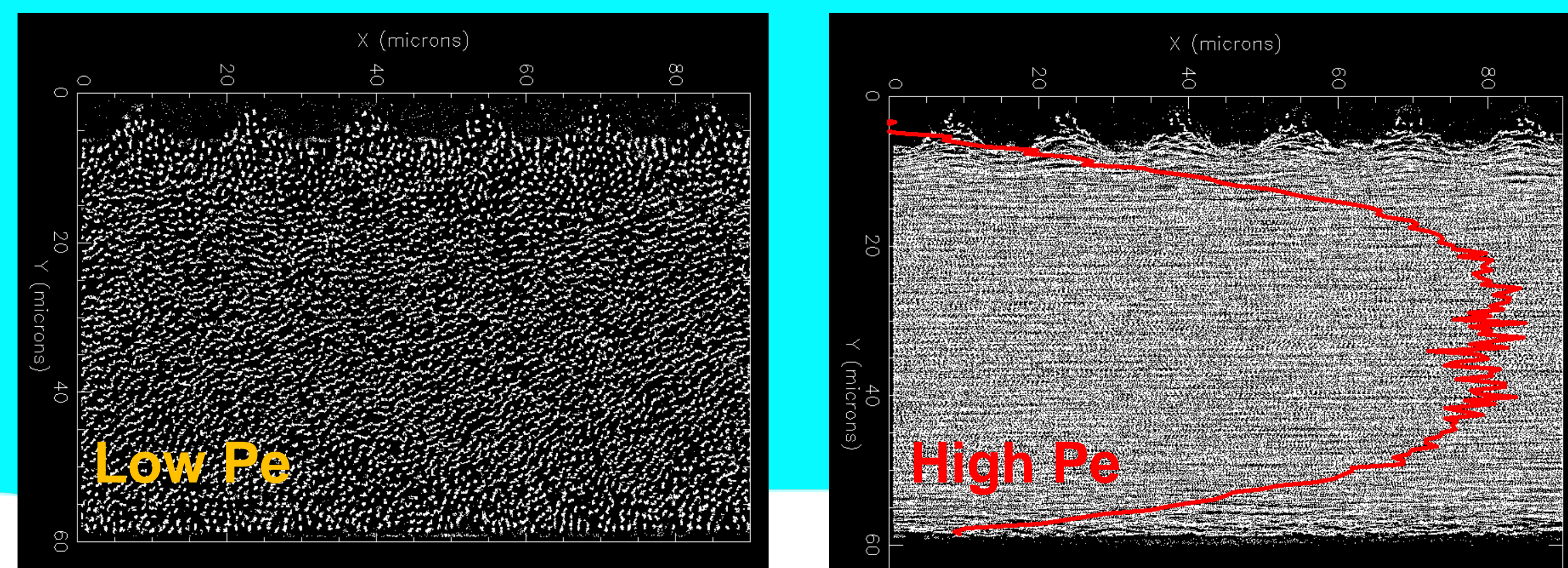
flow speeds: 0.1 – 10 μm/s

movies: 500-1000 frames per condition

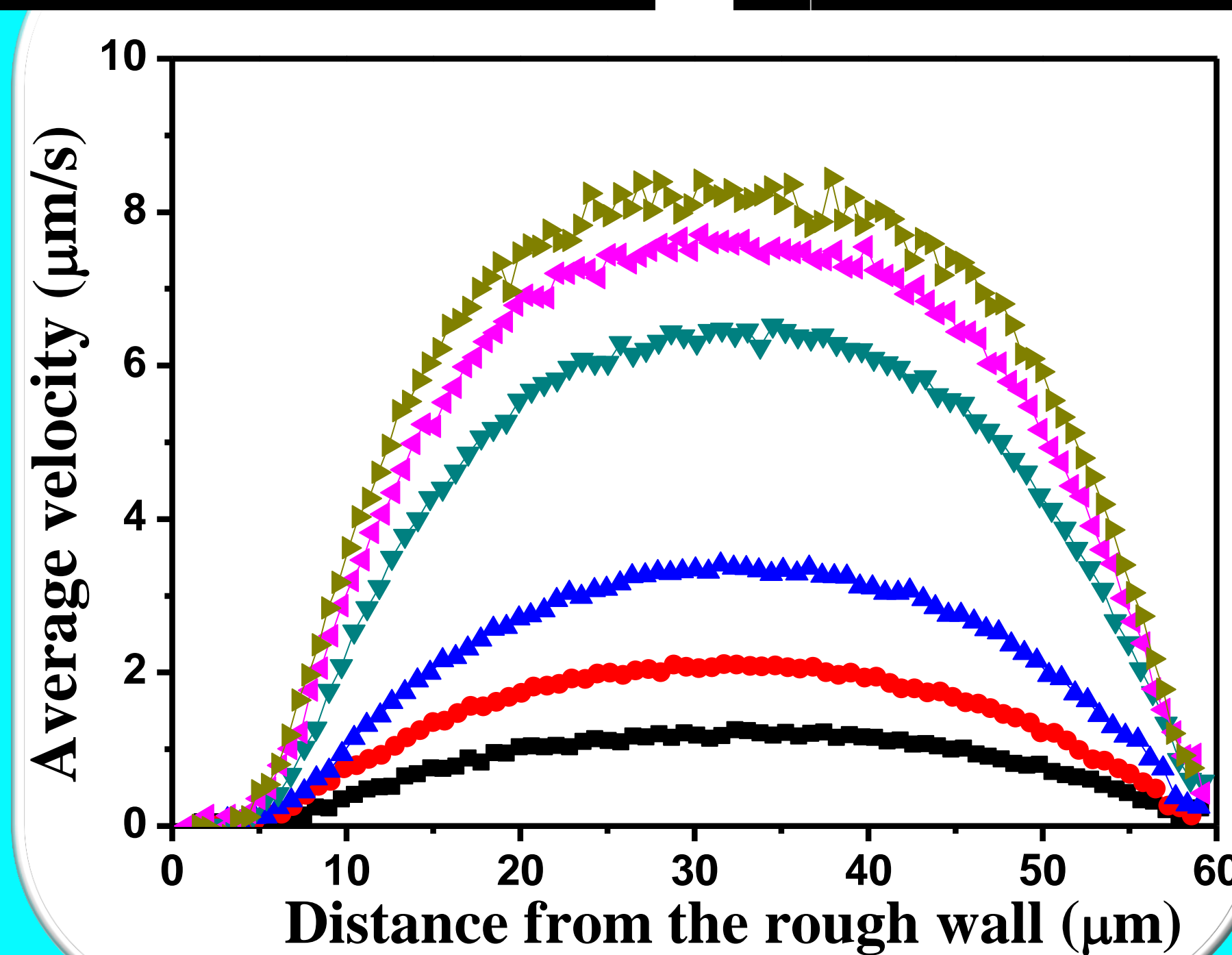
### measurables:

1. local particle number density
2. local mean velocity along flow direction
3. Mean Square Displacement normal to flow:  $\langle \Delta y^2 \rangle = 2 D_{\perp} t$

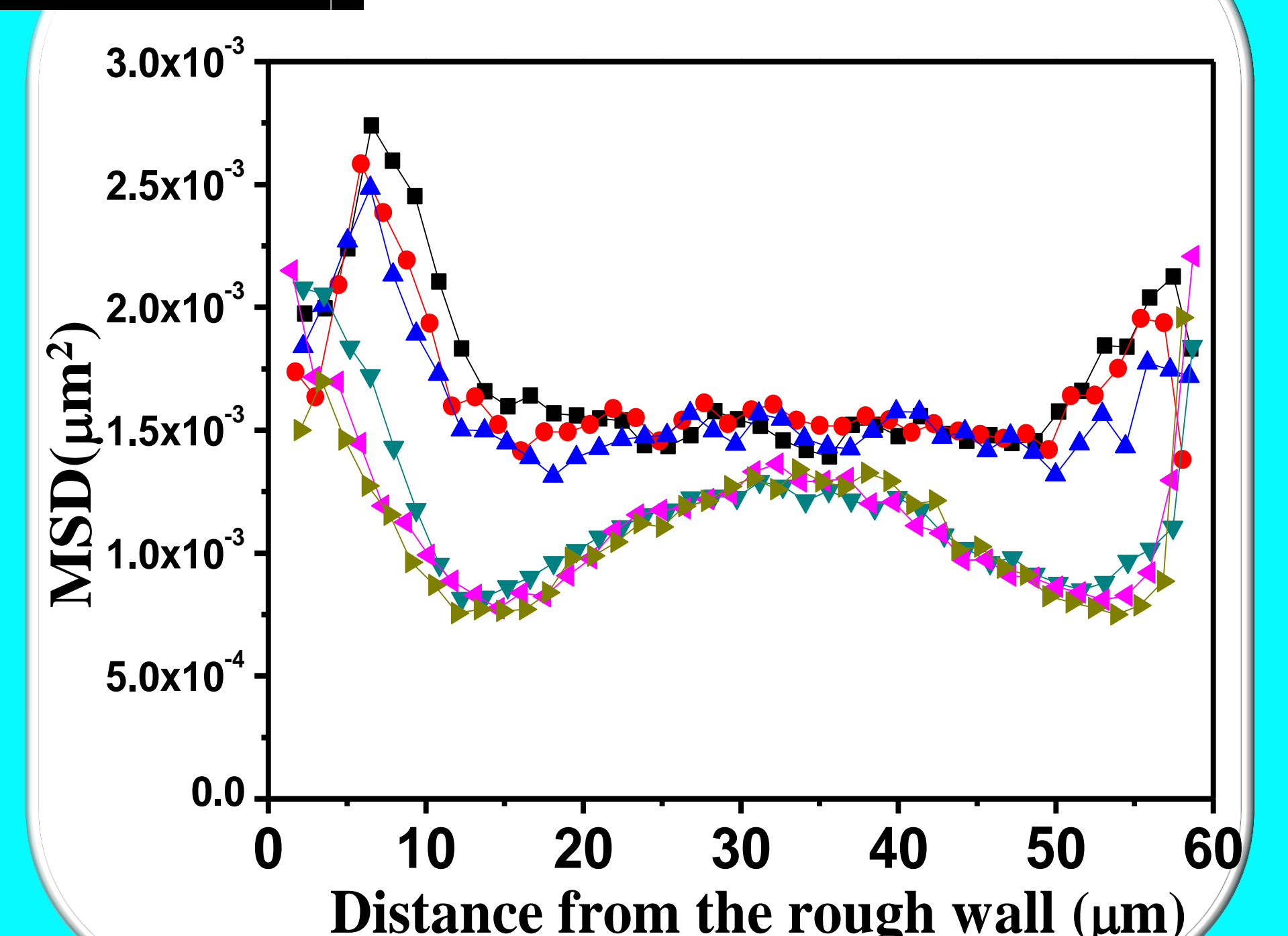
## Observations



Concentration profile



Velocity profile



Apparent diffusivity normal to the flow

## Conclusions

- ❖ Use of both low- and high viscous solvents allows to address a broad range of Péclet numbers, while keeping the maximum flow velocity low enough for particle tracking.
- ❖ Separating the diffusive displacements from the convective ones requires great care, both at high and low Pe.
- ❖ Velocity profiles are nearly parabolic. Slip is always suppressed at the rough wall.
- ❖ The dependence of  $D_{\perp}$  on Pe and the distance relative to the walls still needs to be understood.